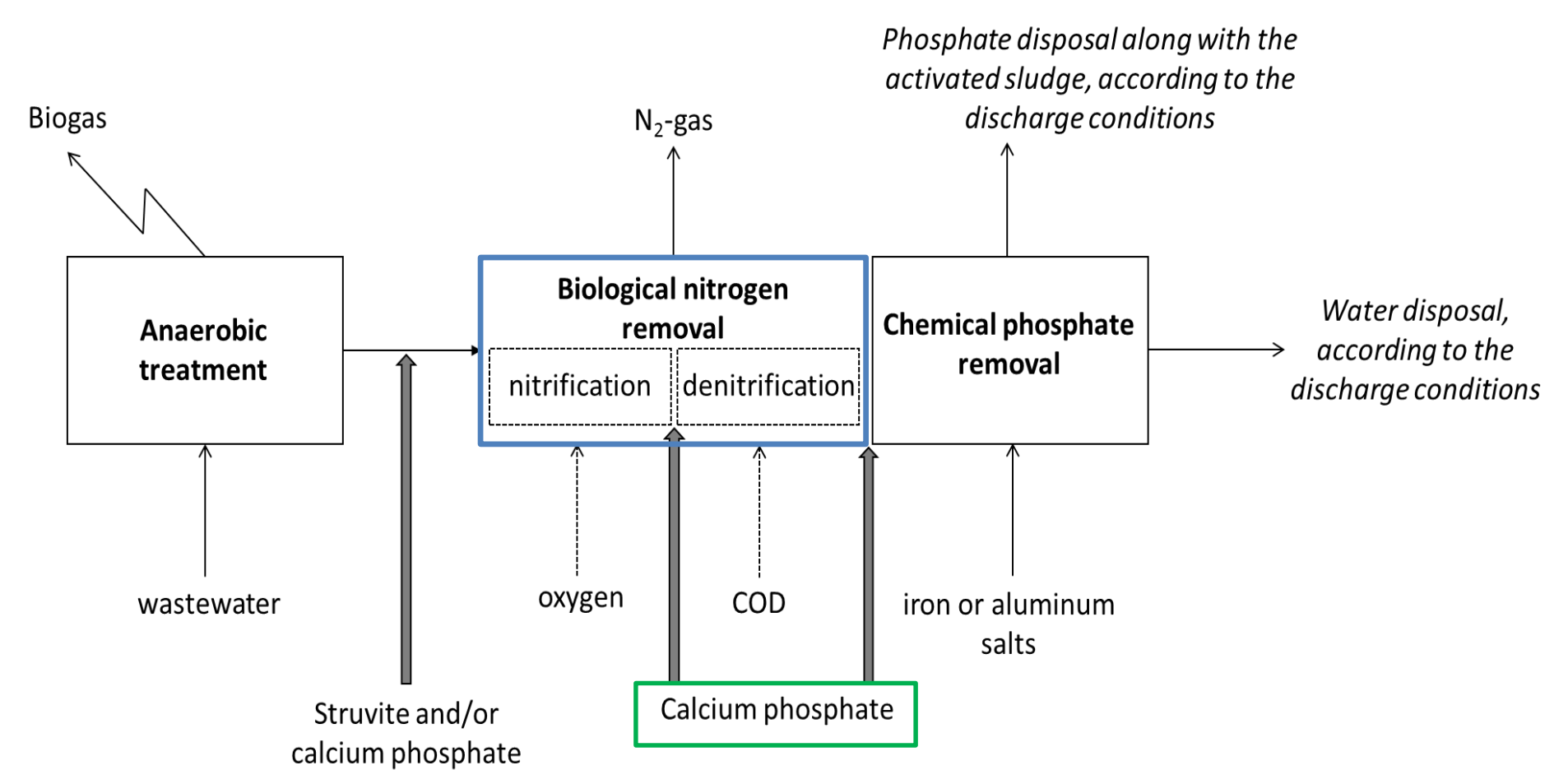


P-Recovery 2.0 – Phosphate recovery after nitrogen removal

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Project goal:

Wastewater from potato processing industry is of valuable interest for **phosphate recovery**. Struvite ($\text{MgNH}_4\text{PO}_4 \cdot 6\text{H}_2\text{O}$) precipitation is applied successfully on some anaerobic treated wastewaters, but it has a rather low commercial value. **Calcium phosphate** may be a more appropriate alternative for re-use applications, at least if it is harvested in a pure, qualitative product.



Methodologies:

- A collected anaerobic treated effluent from a potato processing plant was characterized as follows: pH 7.3; $\text{NH}_4^+\text{-N}$ 145 mg/L; K^+ 754 mg/L; Ca^{2+} 58 mg/L; Mg^{2+} 55 mg/L; $\text{PO}_4^{3-}\text{-P}$ 83 mg/L and TIC (Total Inorganic Carbon) 396 mg/L.
- With short batch experiments the optimal conditions (Ca/P ratio, pH, influencing ions,...) for calcium phosphate precipitation are estimated. Long term experiments are performed on continuously fed and stirred tank reactors.

Results:

- Removing all **TIC** improved recovery of phosphate. In the absence of TIC and starting from pH 8.5, magnesium phosphate precipitated. In the presence of TIC also calcium carbonate seems to precipitate. Increasing the pH with Na_2CO_3 1M invariably led to low phosphate recoveries. The quick formation of soluble complexes as $\text{Ca}_2\text{HPO}_4\text{CO}_3$ and $\text{Ca}_2\text{PO}_4\text{CO}_3^-$ is presumed (Pan and Darvell, 2010).
- No struvite is precipitating within the absence of **ammonium**. At pH 8.5, the precipitate appears to be pure calcium phosphate with a good yield of phosphate removal (75%) at a $[\text{Ca}^{2+}]/[\text{P}]$ ratio of 1.5. Magnesium phosphate precipitation started from pH 10.

Conclusion:

The removal of the buffering compounds ammonium and bicarbonate seems to pave the way to phosphate removal as calcium phosphate at rather low pH levels. The removal of both can be achieved with the **biological nitrification process**. In that case, the TIC/TAN (Total Ammonium Nitrogen) ratio is of importance:

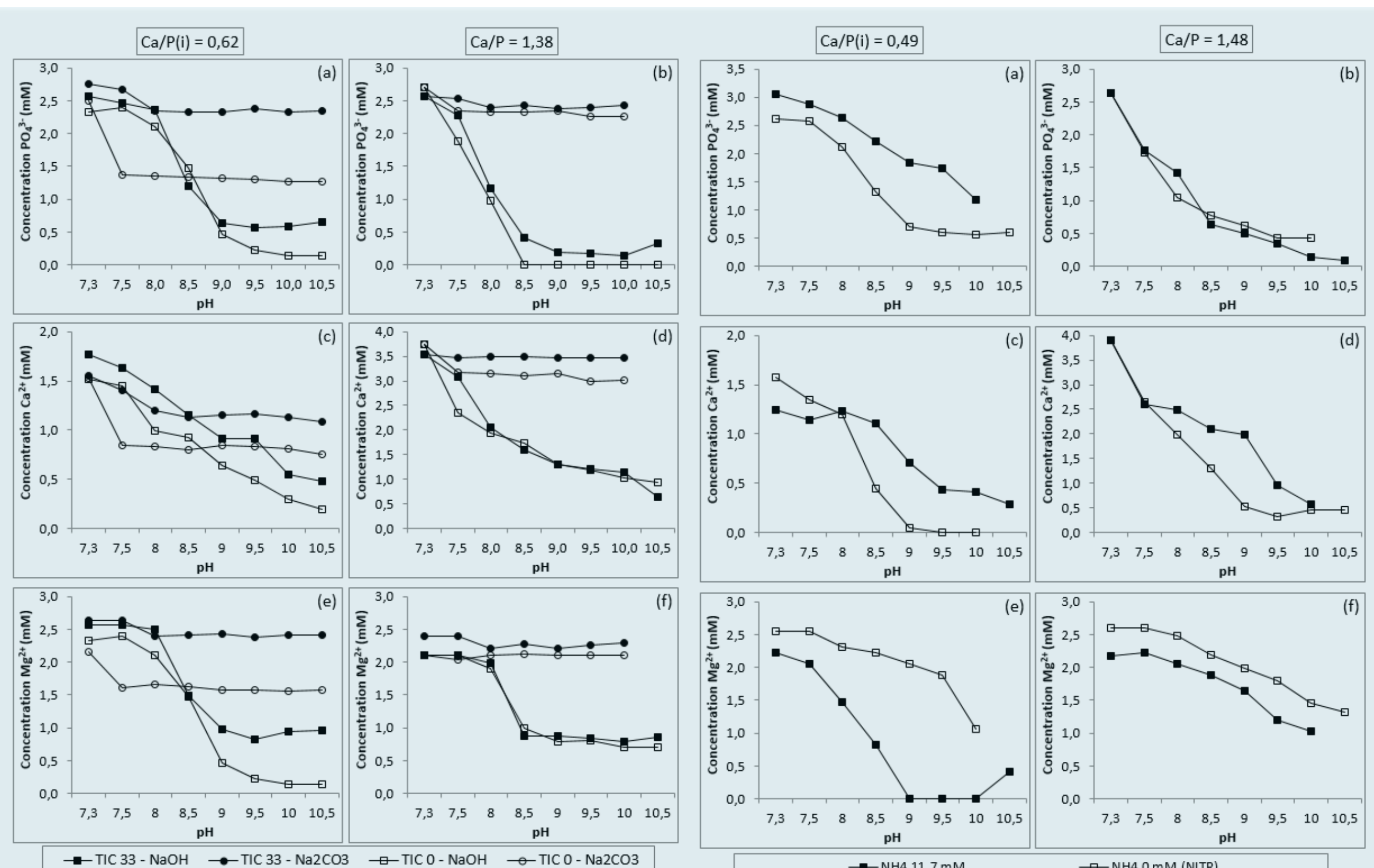
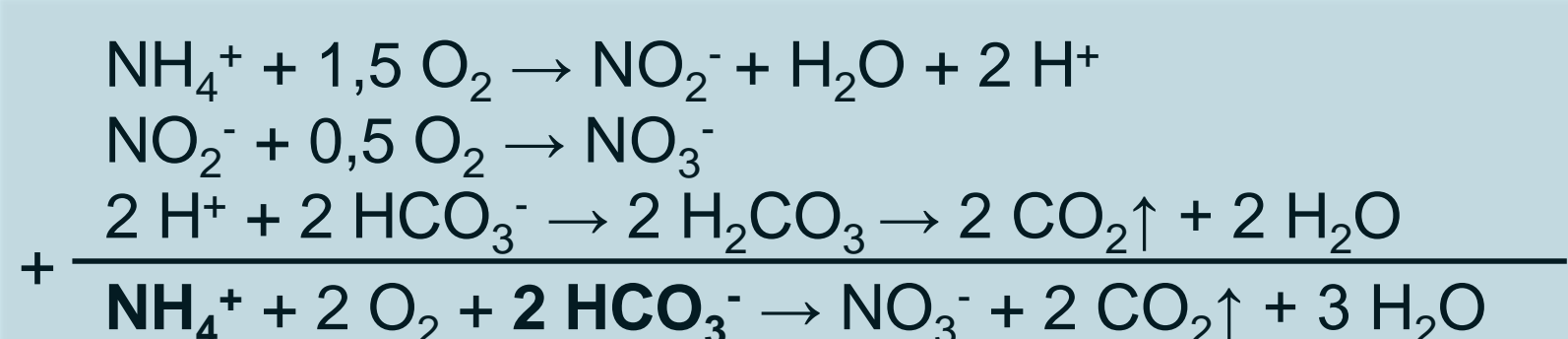


Figure 1 Residual ion concentrations after 1 hour of reaction time when increasing the pH with NaOH 1M or Na_2CO_3 1M of the original the wastewater (see experiment 1, TIC = 33 mM) and after removing TIC (TIC = 0) by aeration under a constant pH; the experiment was carried out without ($[\text{Ca}^{2+}]/[\text{P}]$ ratio = 0.62) and with prior addition of extra Ca^{2+} ions ($[\text{Ca}^{2+}]/[\text{P}]$ ratio = 1.38).

Figure 2 Residual ion concentrations after 1 hour of reaction time when increasing the pH with NaOH 1M of the wastewater after nitrification (NH_4 0 mM, TIC 9,6 mM) and of the wastewater with a reduced TIC concentration by aeration (NH_4 11,7 mM, 9,6 mM TIC); the experiment was carried out without ($[\text{Ca}^{2+}]/[\text{P}]$ ratio = 0.49) and with prior addition of extra Ca^{2+} ions ($[\text{Ca}^{2+}]/[\text{P}]$ ratio = 1.48).

It is concluded that the nitrification of anaerobic treated wastewater will result in the precipitation of calcium phosphate with no/less struvite and carbonate interferences. Furthermore, smaller volumes of alkali are necessary to achieve the required pH increase in comparison with the currently applied struvite process.

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